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 e-mail: raevalentina1@gmail.com

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);

$L(x)$ ($\Delta h^E(x,T)$ - $L(x,T)$)

[1].

[264]. $\Delta h^E(x,T) = L_i^0(T)$.

$\Delta h^E(x,T)$ [116]

14].

$L(x,T)$ (1). 1) $\left(\frac{\partial \Delta h^E(x)}{\partial T}\right)_P > 0$;

[8, 9]. 2) $\left(\frac{\partial \Delta h^E(x)}{\partial T}\right)_P < 0$;

() 3) $\left(\frac{\partial \Delta h^E(x)}{\partial T}\right)_P = 0$.

[8, 10].

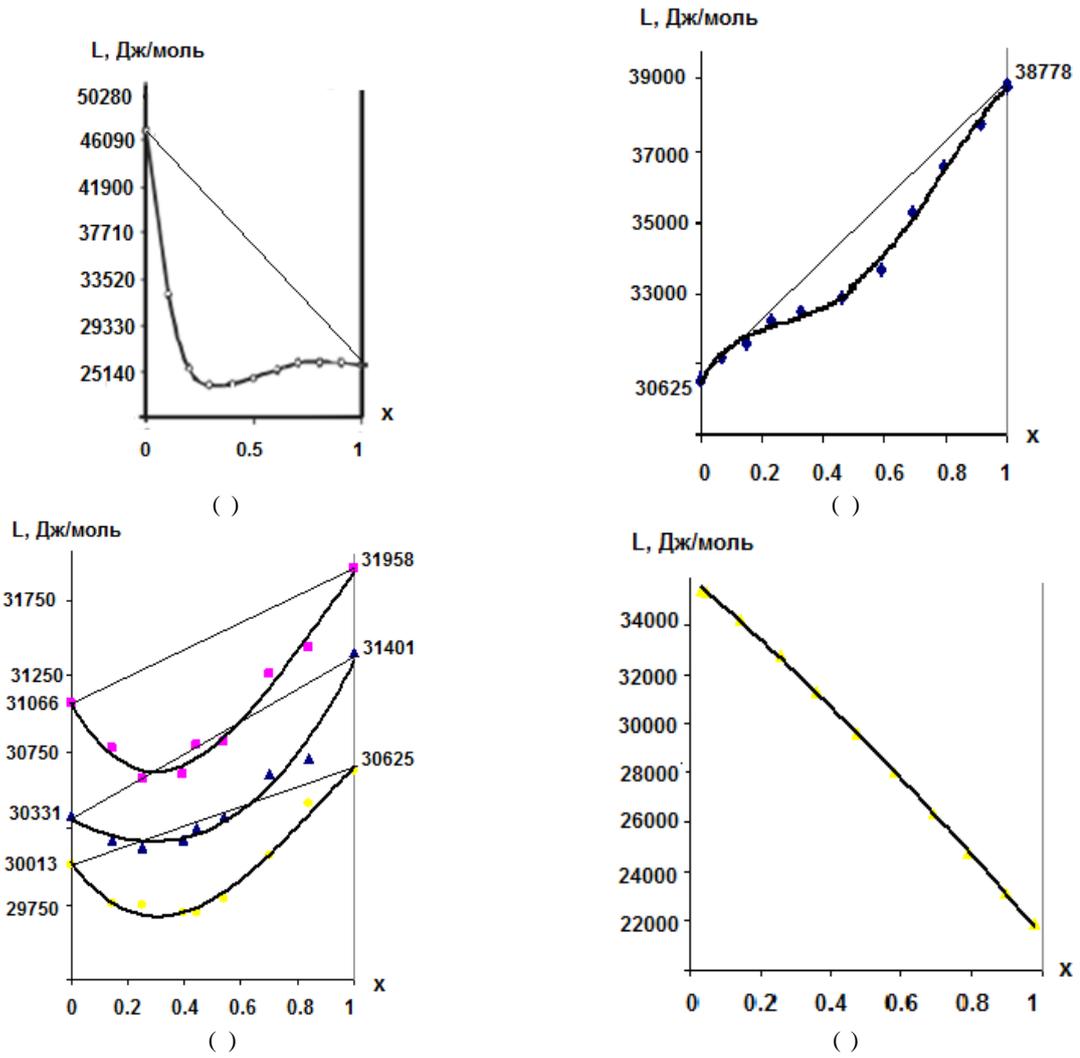
;

$L = \bar{L}_1 x_1 + \bar{L}_2 x_2$, (1) $\left(\frac{\partial \Delta h^E}{\partial T}\right)_{P,x} = \Delta c_P^E$.

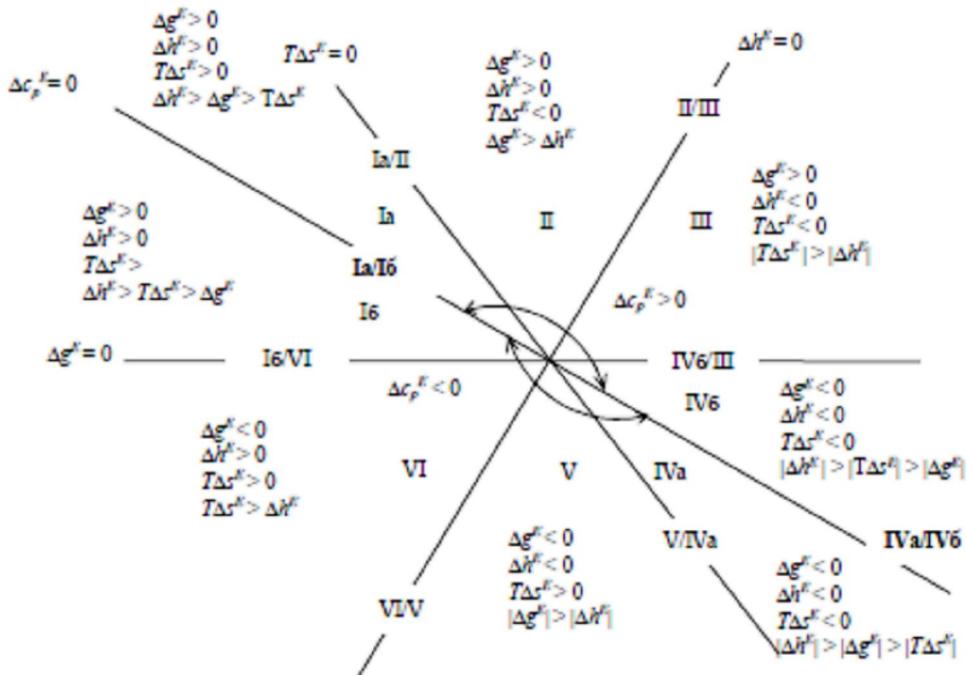
$\bar{L}_i = L_i^0 + \bar{L}_i^E = L_i^0 - \bar{h}_i^E$.

$\Delta c_P^E(x) \geq 0$ $\Delta c_P^E(x) \leq 0$,
 $\Delta c_P^E(x) [14, 15]$.
 1) 2).

$\Delta h^E(x)$:
 $L = (L_1^0 x_1 + L_2^0 x_2) - \Delta h^E = L^a - \Delta h^E$, (2) [14],
 $\Delta h^E = \bar{h}_1^E x_1 + \bar{h}_2^E x_2$
 $\Delta h^E(x) = \Delta c_P^E(x)$ (2)



. 1.
) HF () ó BrF₃ (1-) [5];) () ó (1-), 760 . . [6];
) () ó (1-) 380, 570 ♦♦♦ 760 . . [6];
) () ó (1-) 298.15 [7].



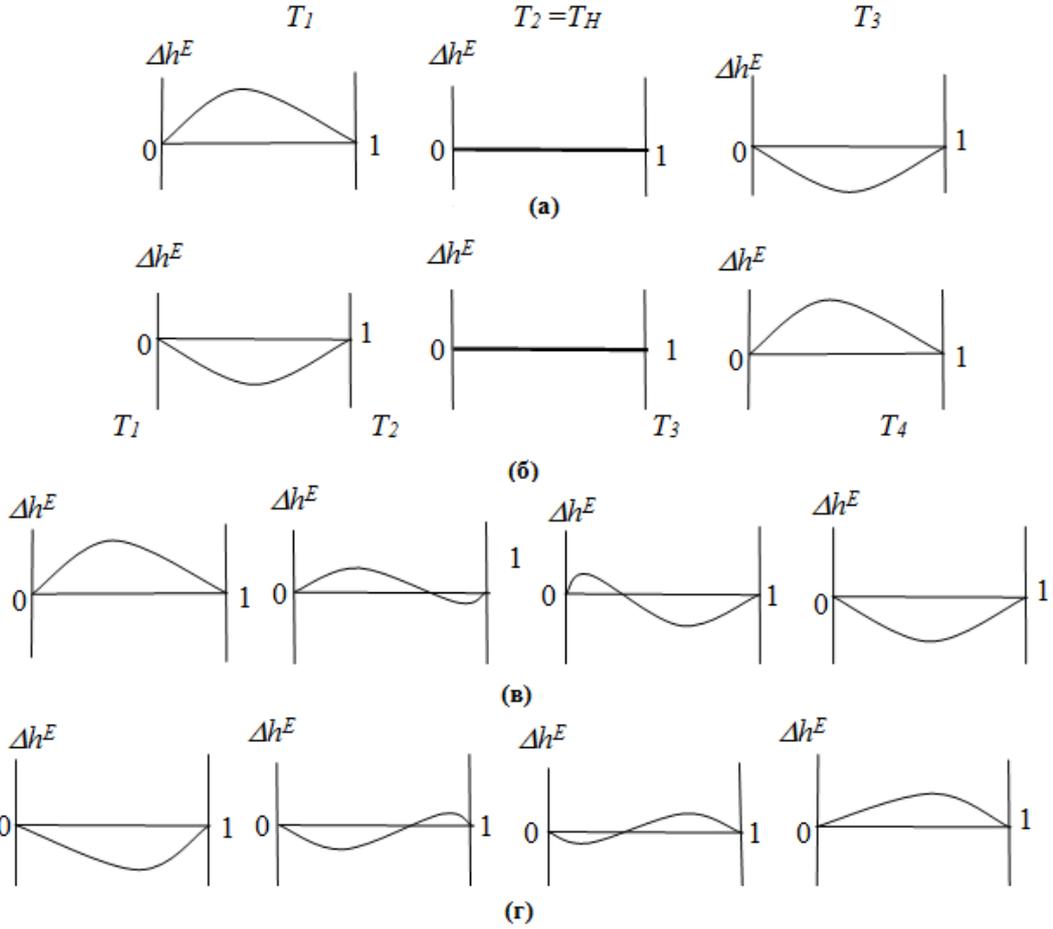
. 2.

[14616].

$$\Delta h^E(x), \quad (\dots 3 \dots),$$

$$\Delta h^E(x) = 0$$

« » , (. 3 ,), (H) c .



. 3.

),) ;),)
 $T_1 < T_2 < T_3 < T_4$

[3]. - 4) $\left(\frac{\partial \Delta L_i^0}{\partial T}\right)_P > 0; = 0; < 0.$ $\left(\frac{\partial \Delta L_i^0}{\partial T}\right)_P = 0$

$$\Delta L_i^0(T) = L_1^0(T) - L_2^0(T)$$

- 1) $\left(\frac{\partial \Delta L_i^0}{\partial T}\right)_P > 0;$ $L_i^0 = const$ [2]. $L_1^0(T) = L_2^0(T)$
- 2) $\left(\frac{\partial \Delta L_i^0}{\partial T}\right)_P < 0;$ ($\Delta L_i^0 \quad \Delta h^E(x)$.
- 3) $\left(\frac{\partial \Delta L_i^0}{\partial T}\right)_P < 0; = 0; > 0;$ T_H (3, 7, 15, 27, 31) T_L (37-48).
 (39, 43).

$$L(x) = L(x, T) \quad (3)$$

$$\Delta h^E(x) = \bar{L}_1 - \bar{L}_2 - \Delta L_i^0 \quad (2)$$

Exsel,
=const

ChemCad.

$$L_i^0(T) \quad (L = L^a)$$

[16].

$$L(x, T)$$

$$\Delta L_i^0 \quad \Delta h^E(x)$$

$$L(x, T) \quad (5)$$

$$L(x, T)$$

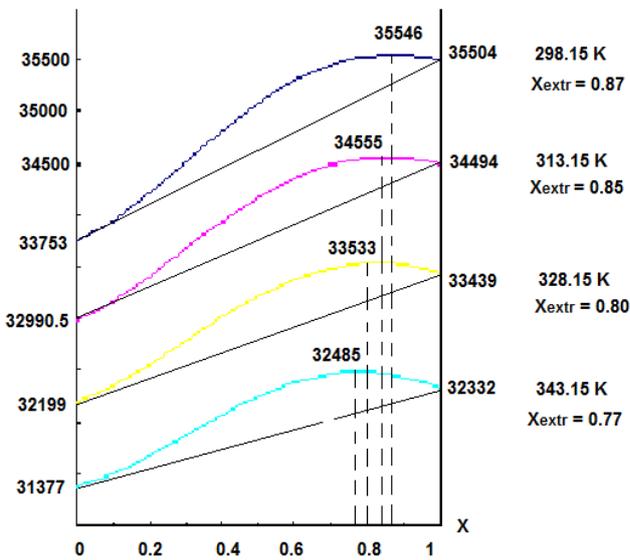
$$\frac{dx_1^{Az}}{dT} = x_1 x_2 \frac{L_1^0 - L_2^0}{RT^2} \quad (4)$$

)

(. 4).

$$L(x)$$

L, Дж/моль



. 5.

() ó

(1-)

$$\Delta h^E(x) \quad [12].$$

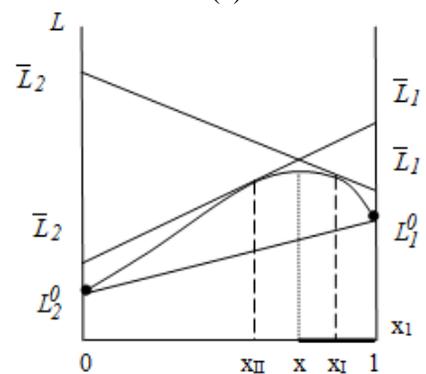
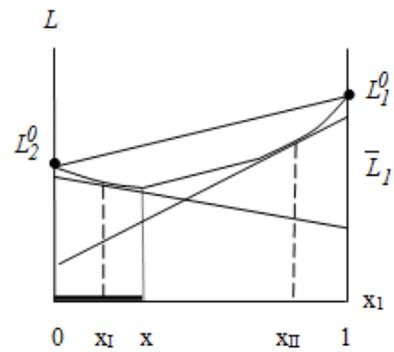
(. 6),

$$0 < x_I < x \quad (. 6) \quad x < x_{II} < 1$$

$$\bar{L}_i \quad \Delta L_i^0$$

x_{II}

(3)



()

$$\frac{dx_1^{Az}}{dT} = \frac{x_1 x_2}{1 - \frac{\partial y_1}{\partial x_1}} \left[\frac{\bar{L}_1 - \bar{L}_2}{RT^2} \right] \quad (8):$$

(3)

(1)

$$\Delta h^E(x) > 0;$$

$$\Delta h^E(x) < 0.$$

$$L = L^a$$

$$\Delta h^E(x) \neq 0.$$

[9, 16].

$$L = L^a$$

(3),

L_D

$$Q = D(R+1)L_D,$$

$$L(x) \quad P=\text{const} \quad T_D=\text{const}.$$

$$D \text{ ó } , R \text{ ó } , L_D \text{ ó } T_D.$$

(5)

$$L_D \approx L_i^0.$$

$$L \approx L^{ad}.$$

$$\Delta h^E, \quad (2),$$

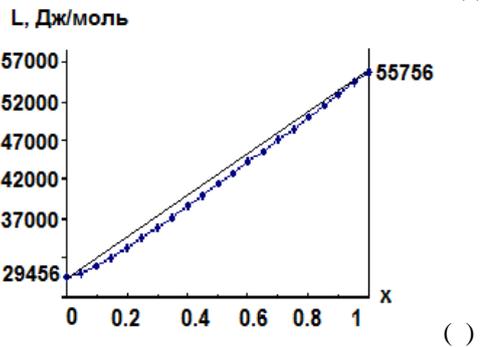
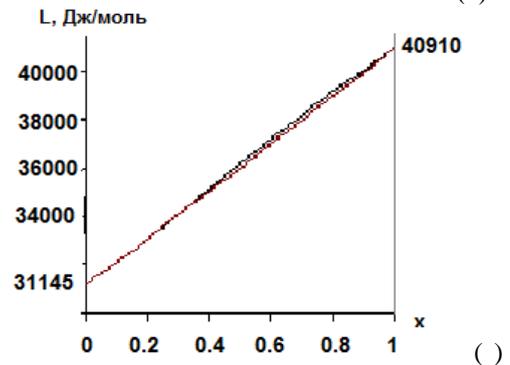
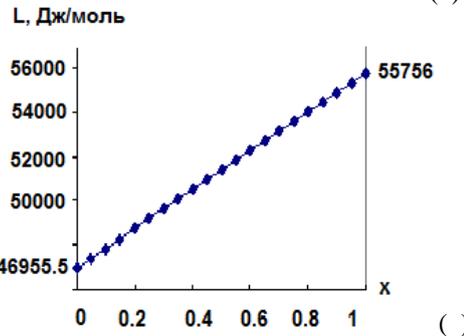
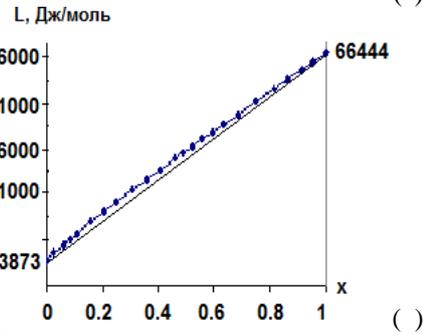
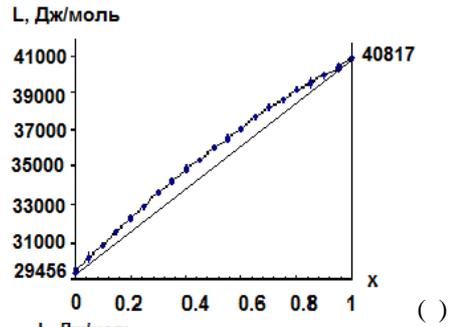
$$\Delta h^E \quad L$$

. 8.

[4]

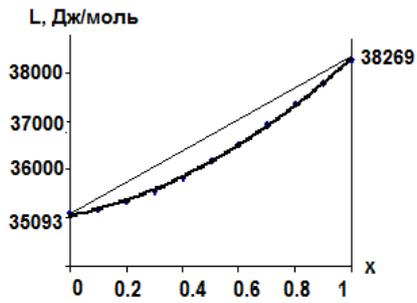
$$\Delta h^E(x,T)$$

$$L(x,T)$$

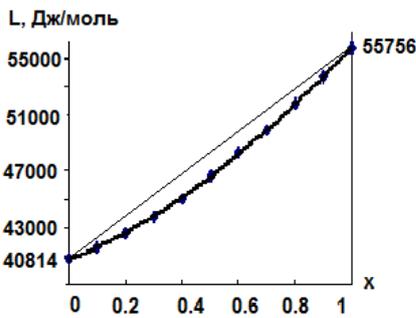


. 7.

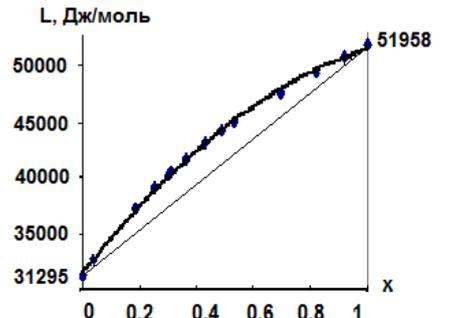
a) () ó , 298.15 : (1-) [17]; () ó (1-) [12]; () ó (1-) [18]; () ó (1-) [12]; () ó (1-) [17].



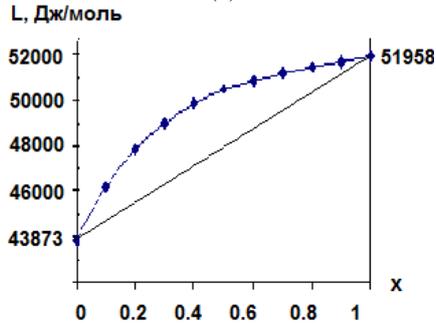
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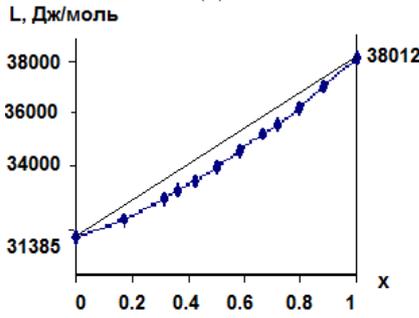
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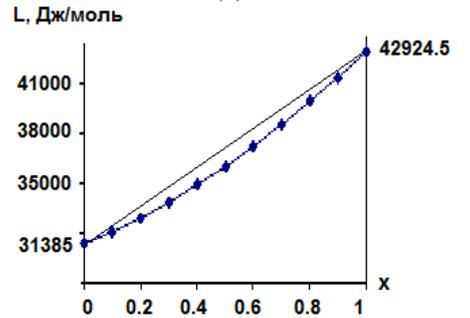
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()



()



()

. 8.

$L(x)$

, 298.15 :

() ó
) () ó
) () ó

(1-) [19];) 2- () ó
(1-) [12];) () ó
(1-) [12];) () ó

(1-) [17];
(1-) [12];
(1-) [12].

$L(x)$

(11-03-00295).

L ó ; T_L ó ; / , ó ; ; T_H ó ; ; ó ; ; Δh^E ó ; / ; \bar{L}_i^E ó ; / .

ó ; A_z ó ; D ó ; $i, 1, 2$ ó ; 0 ó

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VAPORIZATION HEAT OF BINARY MIXTURES

V.M. Raeva

M.V. Lomonosov Moscow State University of Fine Chemical Technology, Moscow, 119571 Russia

@Corresponding author e-mail: raevalentina1@gmail.com

The concentration dependences of integral vaporization heats of binary mixtures were calculated for atmospheric pressure with the use of experimental data. The character of changes of these dependencies under the influence of varying temperature was analyzed.

Key words: *binary mixture, azeotrope, heat of mixing, heat of vaporization of a substance, integral molar latent heat of vaporization, energy consumption for separation.*